ERRATA

W. SZABLEWSKI, Inkompressible turbulente temperaturgrenzschichten mit konstanter wand-temperatur, *Int. J. Heat Mass Transfer* 15(4), 673–706 (1972).

Unfortunately there has been a misunderstanding of a correction of the proof. In formula A(11) the second member on the right is to read

$$\frac{1}{\varkappa}\ln\left(\frac{4}{F}\frac{\sqrt{\left(1 + F\frac{v_*y}{v}\right)} - 1}{\sqrt{\left(1 + F\frac{v_*y}{v}\right)} + 1}\right) \quad \text{not} \quad \frac{1}{\varkappa}\ln\sqrt{\left(1 + F\frac{v_*y}{v}\right)}.$$

Note further:

B(1) is to read $\dfrac{1}{\varkappa_T^2}$ not $\dfrac{1}{\varkappa_T}$; and B(9) is to read $-\dfrac{1}{m}$ not $\dfrac{1}{m}$.

D. M. FONTANA, Simultaneous measurement of bubble growth rate and thermal flux from the heating wall to the boiling fluid near the nucleation site, *Int. J. Heat Mass Transfer* 15(4), 707–720 (1972).

1. Page 709, right column, line 14 from below:
   Cylinder 1 should read Copper sheet 4.

2. Page 709, Fig. 2:
   e.m.f. B between terminals a and b should read e.m.f. B between terminals a and c.

3. Page 711, formula (5):

$$Q_l = -2\pi t_p(z_3 - z_2)\left(k\frac{\partial r_a}{\partial r}\right)_{r=r_a} \quad \text{should read} \quad Q_l = -2\pi r_a(z_3 - z_2)\left(k\frac{\partial t_p}{\partial r}\right)_{r=r_a}.$$

C. E. KALB and J. D. SEADER, Heat and mass transfer phenomena for viscous flow in curved circular tubes, *Int. J. Heat Mass Transfer* 15(4), 801–817 (1972):

1. At the bottom left side of page 802, the line "acting on a fluid flowing through a curved tube." should be added.

2. On page 804, in equation (2a), the last term on the left-hand side of the equation should be

$$\frac{V\cos\theta}{R/a + \eta\sin\theta} \quad \text{instead of} \quad \frac{U\sin\theta}{R/a + \eta\sin\theta}$$

3. On page 806, on the right-hand column, the following line should be inserted just above the 14th line from the bottom: "was discretized in this manner at each of"